Viscosity of Ortho-Substituted Aromatic Amines

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Viscosity measurements were carried out on eight ortho-substituted aromatic amines at 293, 298, 303, 308, 310, 313, 318, 323, and 372 K temperatures. The activation enthalpy of viscous flow was determined. The viscosity in the 293–373 K range can be calculated within an error of 6% from the average activation enthalpy of related compounds (alkylated derivatives).

No viscosity data can be found in the literature relating to ortho-substituted aromatic amines which are liquids at ambient temperature, expect for aniline and o-toluidine. The empirical or semiempirical correlations proposed for the calculation of viscosity proved useless for our purposes. This is so partly because there is no nitrogen increment published for Thomas' method (1), and the effects of substituents are also unknown. The viscosity of aromatic amines which form associates via hydrogen bonds can be calculated only with large error with Souders' method (2).

The ortho 2,6-disubstituted aromatic amines are indispensable intermediates in the pesticide chemistry.

Therefore, the knowledge of their viscosity and the temperature dependence of their viscosity is a must.

Experimental Section

The purity and density data of the aromatic amines tested, aniline (A), *o*-toluidine (OT), 2-ethylaniline (OEA), 2,6-dimethylaniline (DMA), 2-methyl-6-ethylaniline (MEA), 2,6-diethylaniline (DEA), 2-chloroaniline (KA), and 2-chloro-6-methylaniline (KMA), are listed in Table I.

The dynamical viscosity of the above aromatic amines was determined by a Type BH Hoeppler viscosimeter.

The time of fall of the ball between the two extreme works was determined with a digital timer accurate to 0.1 s which gave an error in the measurement of viscosities of $\pm 0.1\%$. Temperature control using a calibrated thermometer was better than ± 0.1 K. Viscosities were determined in the 293–372 K range, at nine temperature settings.

The densities of the aromatic amines were measured by pycnometry taking into account volume changes of the pycnometer at the higher temperatures. Thus the error is about ± 0.001 g/cm³.

Results and Discussion

Measured viscosity values are listed in Table II. The activation enthalpy of viscous flow reads as

$$H^* = -RT^2 (d \ln \eta / dT) p \tag{1}$$

After integration and rearrangement

$$\eta = A \exp(\Delta H/RT) \tag{2}$$

After linearization

$$\ln \eta = \ln A + \Delta H / RT \tag{3}$$

It can be seen from eq 3 that a linear relationship exists between the logarithm of dynamical viscosity and the reciprocal absolute temperature. This notion is sustantiated by the mea-

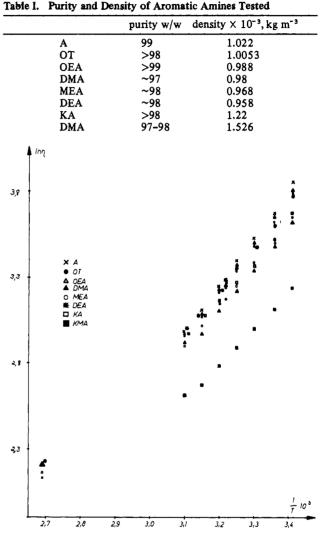


Figure 1. Temperature dependence of the viscosity of aromatic amines.

sured data (cf. Figure 1). The measured values fit a straight line. The coefficients of this straight line can be obtained by regression analysis (cf. Table III).

$$Y = B_0 + B_1 X \tag{4}$$

It can be seen in both Figure 1 and Table III that the viscous of aromatic amines at constant temperature—except those of the chloro derivatives—are very similar. Therefore, the viscosities of the alkylated derivatives can be averaged. The coefficients of eq 4 can be also determined from the averaged data. Those values yield the intercept and the activation enthalpy of viscous flow (cf. Figure 2).

$$\ln A = -3.5796$$

$$\Delta H^* = 17.705 \text{ kJ mol}^{-1} \text{ K}^{-1}$$

Thus, the viscosity of ortho-substituted alkylated aromatic amines can be calculated by the equation

$$\eta = 2.789 \times 10^{-2} \exp(17705/RT)$$
(5)

10

4

27

2.8

2.9

30

Figure 2. Average viscosity of alkylated aromatic amines.

| | dynamical viscosity, mPa·s | | | | | | | | | | |
|------------------------------|----------------------------|-------|------------|-------------------|-------------------------------------|--|--|---|---|--|--|
| | 293 K | 298 K | 303 K | 308 K | 311 K | 313 K | 318 K | 323 K | 372 | ĸ | |
| A | 47.08 | 39.95 | 34.20 | 30.00 | 26.30 | 25.97 | 22.55 | 20.00 | 9.1 | | |
| OT | 44.50 | 37.25 | 32.55 | 28.20 | 25.60 | 24.85 | 21.50 | 19.40 | 8.9 |) | |
| OEA | 45.00 | 38.50 | 33.25 | 29.15 | 25.90 | 25.24 | 21.80 | 19.50 | 9.1 | | |
| DMA | 37.40 | 32.60 | 28.32 | 25.00 | | 22.26 | 19.50 | 18.57 | | | |
| MEA | 38.70 | 33.50 | 29.50 | 26.00 | 23.90 | 23.52 | 20.45 | 18.20 | 8.7 | | |
| DEA | 43.70 | 36.50 | 32.45 | 28.50 | 26.80 | 25.45 | 22.00 | 20.00 | 9.3 | | |
| KA | 39.44 | 34.00 | 29.31 | 26.26 | | 23.68 | 21.50 | 19.56 | | | |
| | | | | | | | | | | | |
| КМА | 25.60 | 22.63 | 20.14 | 17.99 | | 16.14 | 14.50 | 13.65 | | | |
| KMA 2/m ^{Pa.s} / | 25.60 | 22.63 | 20.14 | 17.99 * | | Coefficients of Northalpy of N | of the Linea /iscous Flow | r Regression M v Calculated fr | om Coel | fici | |
| | 25.60 | 22.63 | 20.14 1 | 17.99 | Activation | Coefficients of Enthalpy of A | of the Linea V is cous Flow B_1 | r Regression M v Calculated fr H, ^a kJ mol ⁻¹ | rom Coel R ^b | fici N ^o | |
| | 25.60 | 22.63 | 20.14 | 17.99 | Activation A | Coefficients of Enthalpy of V B_0 -3.8974 | of the Linea $V_{\rm iscous}$ Flow B_1 2246.72 | r Regression M v Calculated fr H, ^a kJ mol ⁻¹ 18.685 | rom Coel R ^b 0.994 | ficio N ^o 9 | |
| | 25.60 | 22.63 | 20.14 | 17.99 | Activation A OT | Coefficients of Enthalpy of V B_0 -3.8974 -3.7751 | $\frac{B_1}{2246.72}$ | r Regression M v Calculated fr H, ^a kJ mol ⁻¹ 18.685 18.250 | rom Coel <i>R^b</i> 0.994 0.944 | ficio N ^o 9 | |
| | 25.60 | 22.63 | 20.14 | 17.99 | Activation A OT OEA | Coefficients of Enthalpy of V B_0 -3.8974 -3.7751 -3.7683 | $\frac{B_1}{2246.72}$ | r Regression M v Calculated fr H, ^a kJ mol ⁻¹ 18.685 18.250 18.281 | rom Coel <i>R^b</i> 0.994 0.944 0.993 | ficio N ^o 9 9 9 | |
| | 25.60 | 22.63 | 20.14 | 17.99 | Activation A OT OEA DMA | Coefficients of Enthalpy of V B_0 -3.8974 -3.7751 -3.7683 -4.1801 | of the Linea /iscous Flow B ₁ 2246.72 2194.39 2198.07 2282.23 | r Regression M v Calculated fr H, ^a kJ mol ⁻¹ 18.685 18.250 18.281 18.981 | 0.994 0.993 0.997 | 9 9 9 7 | |
| | 25.60 | 22.63 | 20.14 | 17.99 | Activation A OT OEA | Coefficients of Enthalpy of V B_0 -3.8974 -3.7751 -3.7683 | $\frac{B_1}{2246.72}$ | r Regression M v Calculated fr H, ^a kJ mol ⁻¹ 18.685 18.250 18.281 | rom Coel <i>R^b</i> 0.994 0.944 0.993 | ficie N ^e 9 9 | |

Table II. Viscosity of Aromatic Amines

2192.42 DMA -3.69542030.27 16.885 0.998 7 ^a H = enthalpy of viscous flow. ^b R = regression factor. ^c N =number of experimental points.

-3.8292

The average relative error of the viscosities of the aromatic amines tested, calculated by eq 5, is 5.96%.

0.997

7

18.225

Literature Cited

KA

(1) Thomas, L. H. J. Chem. Soc. 1946, 573. (2) Souders, M. J. Am. Chem. Soc. 1938, 60, 154.

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Thermodynamic Properties of Solutions Containing an Aliphatic Amine. 1. Excess Volumes of Binary Systems of Triethylamine with Benzene, Toluene, Ethylbenzene, and Isomeric Xylenes at 313.15 K

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2,4

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3.1

Excess volumes, V^E, of binary mixtures of triethylamine with benzene, toluene, ethylbenzene, and three isomeric xylenes at 313.15 K have been computed from the experimental density data. V^E decreases when an alkyl group is added to the benzene ring. For isomeric xylenes, it follows the order m-xylene > o-xylene > p-xylene.

Introduction

As a part of our investigations on the thermodynamics of binary mixtures (1-3), we considered it worthwhile to study in detail the dependence of each thermodynamic property of the binary mixture of representative aliphatic amines on the nature

| Table I. Physical Properties of Liquids Used |
|--|
|--|

| | density at | 313.15 K | refractive index (298.15 K) | | |
|------------------|------------|---------------------|--------------------------------|-------------------|--|
| solvent | our value | lit. value (6) | our value | lit. value (6) | |
| triethylamine | 0.709 59 | 0.7092 ^a | 1.3980 | 1.398 0b | |
| benzene | 0.857 63 | 0.8576 | 1.4980 | 1.497 92 | |
| toluene | 0.847 25 | 0.8482 | 1. 494 0 | 1.494 13 | |
| ethylbenzene | 0.84940 | 0.8494 | 1.4932 | 1.493 20 | |
| o-xylene | 0.86283 | 0.8633 | 1.5028 | 1.502 95 | |
| <i>m</i> -xylene | 0.847 15 | 0.8471 | 1.4946 | 1.494 64 | |
| p-xylene | 0.843 83 | 0.8436 | 1.4932 | 1.493 25 | |

^a Calculated from the modified Rackett equation (8) with $Z_{RA} = 0.26992$ adjusted to the density value at 298.15 from ref 6. ^b Reference 7.